

## CLAIMS

1. A process for producing polyarylene sulfide,  
comprising: reacting an aromatic dihalide compound  
and an alkaline metal compound in a polar organic  
5 solvent for polymerization under heating, and cooling a  
system including the reaction mixture to recover  
particulate polyarylene sulfide, wherein the system  
after the reaction is gradually cooled at an average  
cooling speed of 0.2 to 1.0 °C /min. selectively in a  
10 temperature range of maximum system-viscosity  
temperature  $\pm 1$  °C.

2. A process according to Claim 1, wherein in the  
reaction under heating, a phase separation agent is  
15 added to a reaction system at a desired time from a  
start to an end of the reaction so as to form a  
liquid-liquid phase separation state including a thick  
phase and a dilute phase of product polymer, and then  
the cooling is started.

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3. A process according to Claim 2, wherein the phase  
separation agent is water.

4. A process according to Claim 3, wherein the alkaline  
25 metal compound is an alkaline metal sulfide and the  
phase separation agent is water;

the reaction under heating includes a preceding

step of reaction at a temperature in a range of 180 °C to 235 °C in the presence of 0.5 to 2.4 mols of water per mol of the charged alkaline metal sulfide to form a prepolymer at a conversion of 50 to 98 mol% of the aromatic dihalide compound, and a subsequent step of adding water so as to provide an amount of water exceeding 2.5 mols and at most 7.0 mols per mol of the charged alkaline metal sulfide in the reaction system and heating the system to a temperature of 245 to 290 °C to continue the reaction; and  
after the reaction, the cooling is started.

5. A process according to any preceding claim, wherein the reaction and the cooling are performed in a reaction vessel equipped at its top with a reflux condenser as a principal cooling means for the cooling.

6. A process according to Claim 5, wherein during the cooling, at least a portion of non-condensable gaseous component is removed from a top gaseous phase in the reflux condenser to enhance a cooling capacity of the reflux condenser.

7. A process according to any preceding claim, wherein the system is cooled at a cooling speed exceeding 1.0 °C /min. outside a temperature range of maximum system-viscosity temperature  $\pm 3$  °C.

8. A process according to Claim 7, wherein the system is cooled at a cooling speed of at least 2.0 °C /min. outside the temperature range of maximum system-viscosity temperature  $\pm 3$  °C.

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9. A process according to any of claims 1 to 6, wherein the system is cooled at a cooling speed exceeding 1.0 °C /min. outside a temperature range of maximum system-viscosity temperature  $\pm 2$  °C.

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10. A process according to Claim 9, wherein the system is cooled at a cooling speed of at least 2.0 °C /min. outside the temperature range of maximum system-viscosity temperature  $\pm 2$  °C.

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11. A process according to any preceding claim, wherein the system is cooled at an average cooling speed of 0.2 to 1.0 °C in the temperature range of maximum system-viscosity temperature  $\pm 2$  °C.